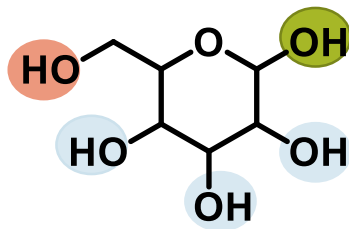


IRON CATALYSIS FOR THE OXIDATION OF UNPROTECTED SUGARS

Dr Laure Benhamou

Normandy Le Havre University

- Traditional strategies



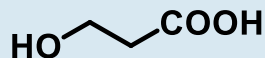
- Polyfunctionality & Selectivity
- Protection / Deprotection

- Green Chemistry & sugars exploitation

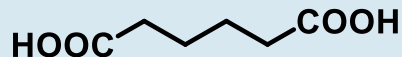
Fermentation

Alcohol: EtOH, *n*BuOH

3-HPA

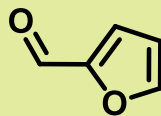


Adipic acid

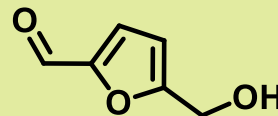


Dehydration

Aromatic derivatives



Furfural

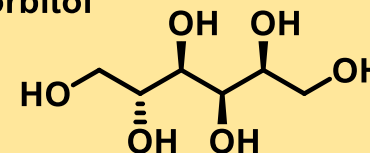


HMF

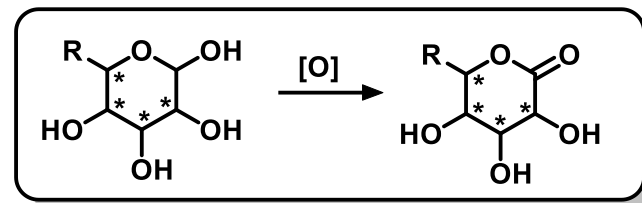
Hydrogenation

Hydrocarbons: benzene, xylene

Sorbitol



- Catalytic Cl-oxidation of unprotected sugars
 - Traditional stoichiometric processes: halogen derivatives
 - Catalytic methodologies



Selected examples

Limitations

Biocatalysis

Gluconolactone
industrial synthesis

Narrow range of
tolerated substrates

Heterogeneous catalysis

Au / H₂O₂ / hν
TiO₂ / O₂ / hν

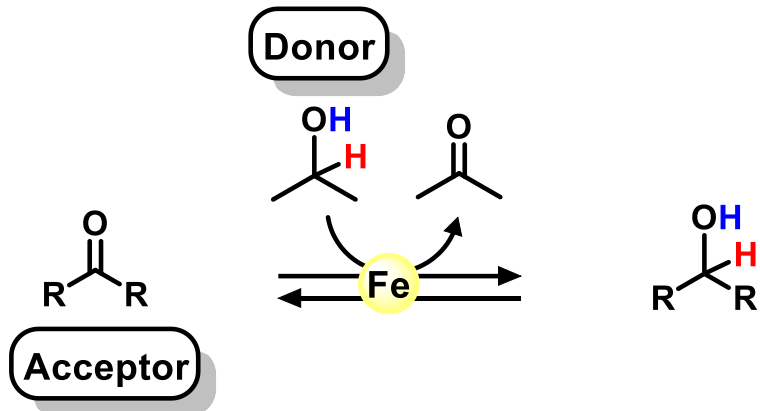
Selectivity

Homogeneous catalysis

TEMPO / NaOCl
Pd catalysis

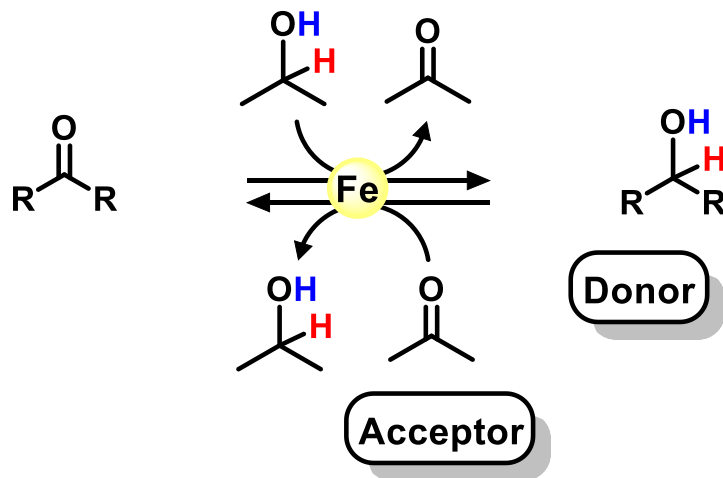
Halogenated agent
Selectivity

- Catalytic transfer hydrogenation (TH)
 - Alternative to direct hydrogenation



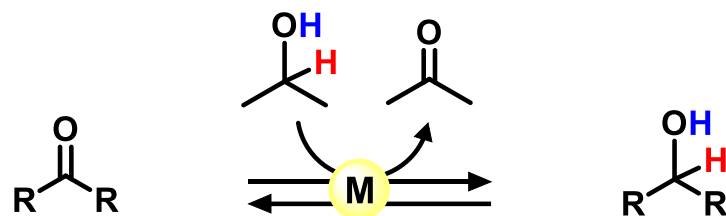
- Simple set-up
- Reversibility

- Catalytic transfer hydrogenation (TH)
 - Alternative to direct hydrogenation



- Simple set-up
- Reversibility
- Strong oxidant free

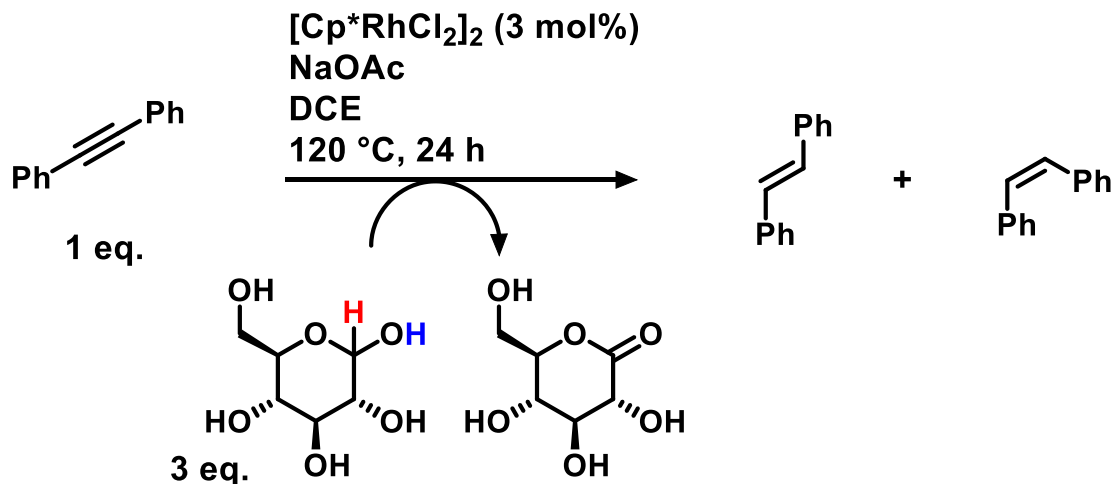
- Catalytic transfer hydrogenation (TH)
 - Alternative to direct hydrogenation



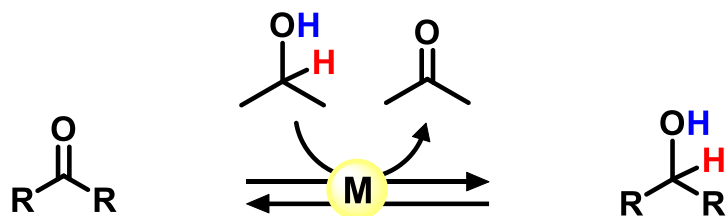
- Simple set-up
- Reversibility
- Strong oxidant free

- Sugar oxidation via catalytic TH : a noble metal matter?

Rhodium



- Catalytic transfer hydrogenation (TH)
 - Alternative to direct hydrogenation



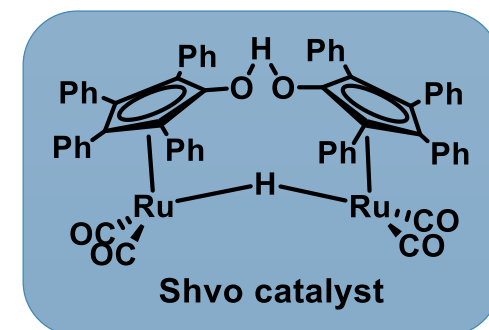
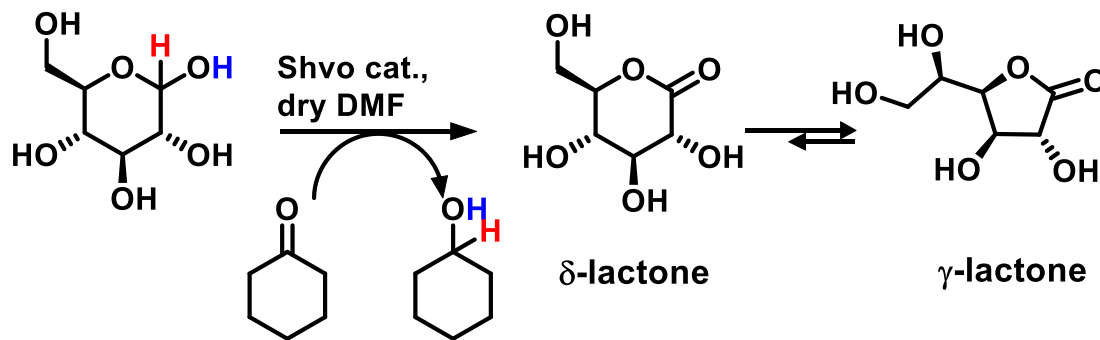
- Simple set-up
- Reversibility
- Strong oxidant free

- Sugar oxidation via catalytic TH : a noble metal matter?

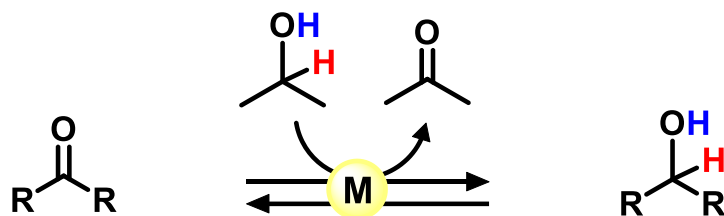
Ruthenium

Kinetic

Thermodynamic



- Catalytic transfer hydrogenation (TH)
 - Alternative to direct hydrogenation



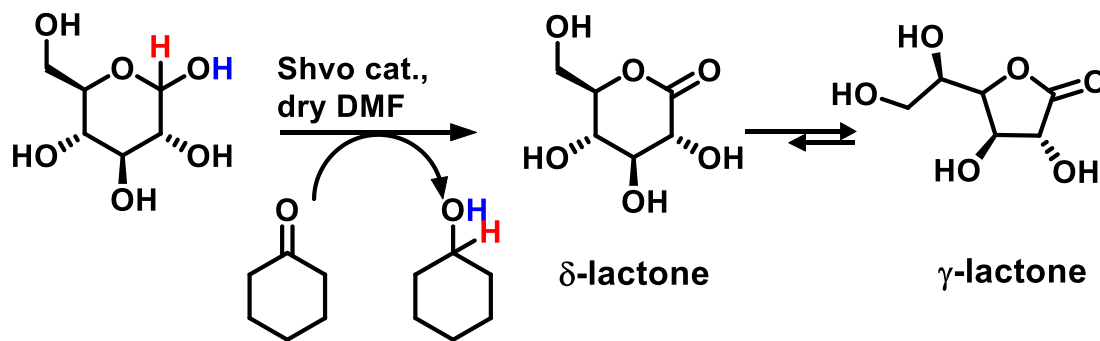
- Simple set-up
- Reversibility
- Strong oxidant free

- Sugar oxidation via catalytic TH : a noble metal matter?

Ruthenium

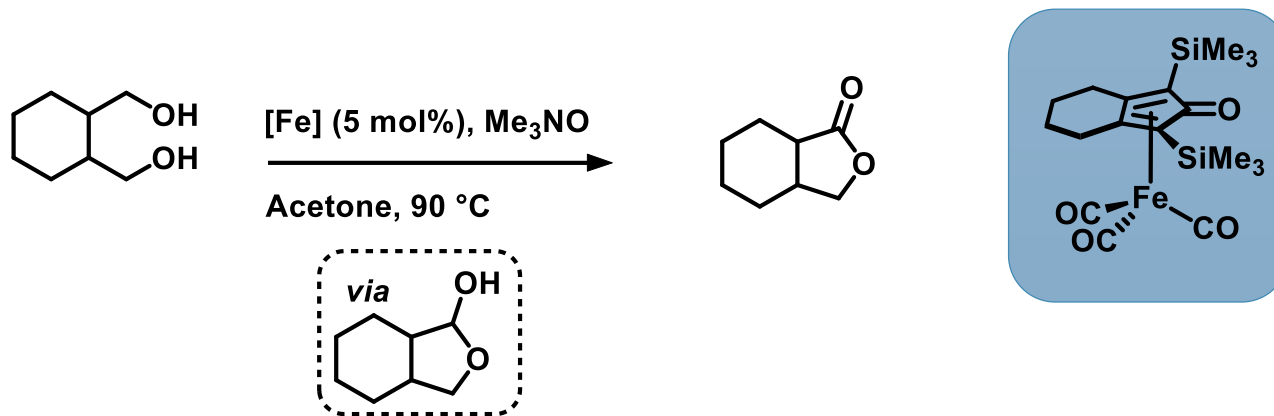
Kinetic

Thermodynamic



- ✓ Excellent selectivity & activity
- ✓ Hexoses oxidation
- ✓ Mild conditions
- Inert condition
- Large excess of acceptor
- Hazardous solvent
- Precious metal

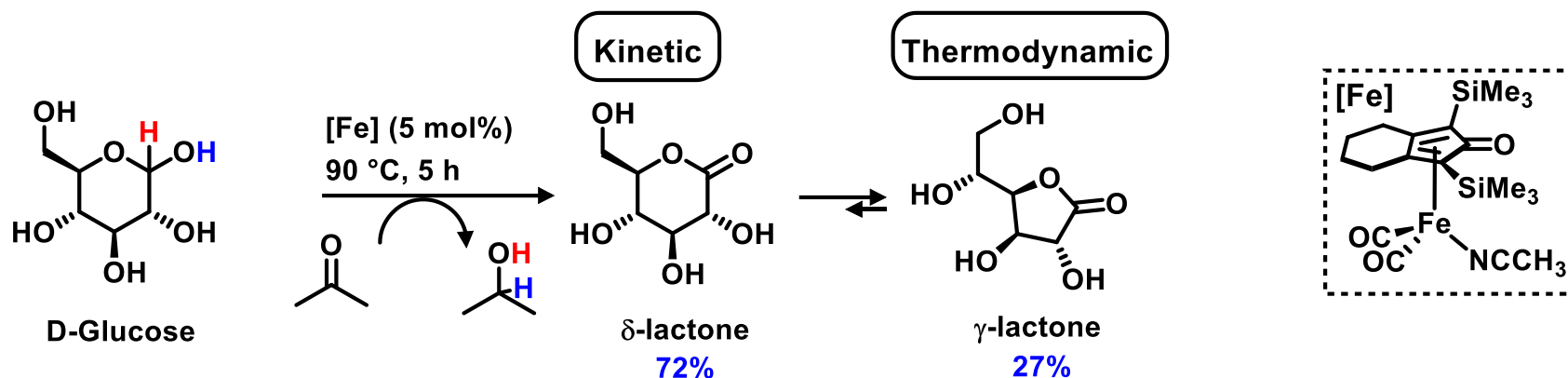
- Knölker catalyst



- Oxidation / reduction of alcohol/ketone derivatives
- Application in hydrogen borrowing transformation
- Analogous to Shvo catalyst
- Air and moisture stable

Optimisation

- Preliminary test

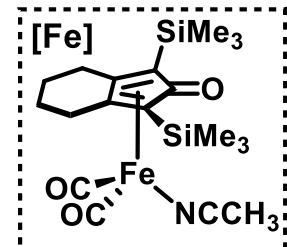
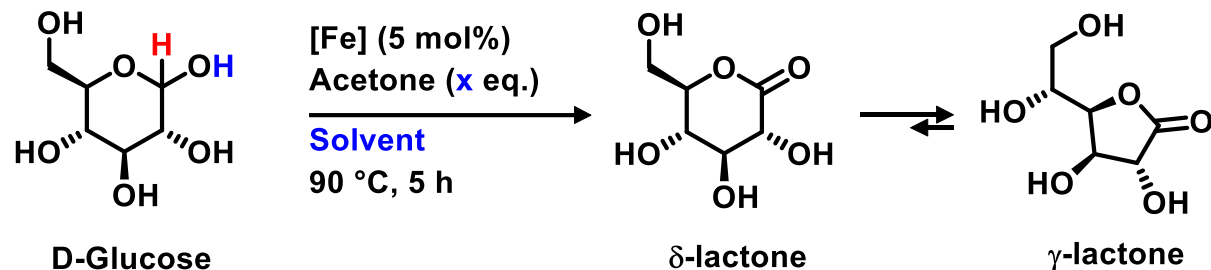


- Complete oxidation of glucose
- Chemo-selectivity for the more reactive anomeric position
- Base and strong-oxidant free
- Full isomerisation in 24 h (+ acetalisation product with acetone)

Decrease the amount of acceptor?

Optimisation

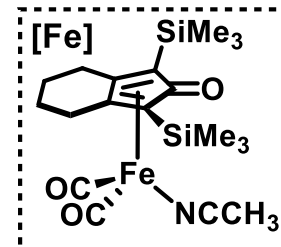
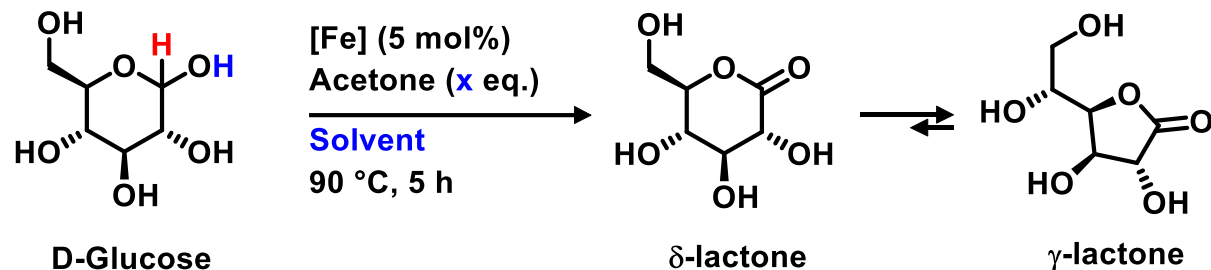
- Solvent screening



Solvent	Acetone (Eq.)	Lactone Yield (%)
H ₂ O	10	0
CH ₃ CN	10	0
CH ₃ CN	100	0
HFIP	10	0

Optimisation

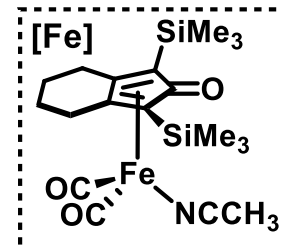
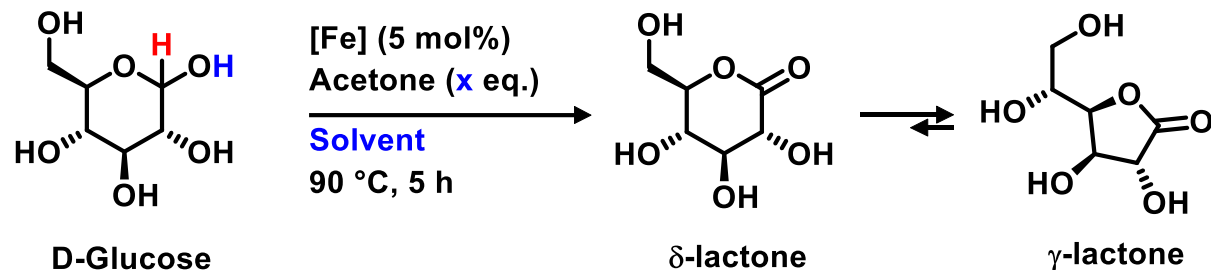
- Solvent screening



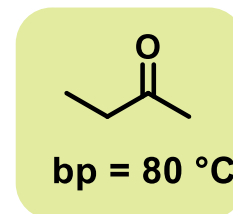
Solvent	Acetone (Eq.)	Lactone Yield (%)
H_2O	10	0
CH_3CN	10	0
CH_3CN	100	0
HFIP	10	0
$\text{CF}_3\text{CH}_2\text{OH}$	10	40
tBuOH	10	90
tBuOH	9	58
tBuOH	7	50

Optimisation

- Solvent screening



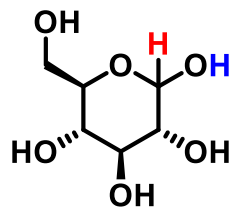
Solvent	Acetone (Eq.)	Lactone Yield (%)
H ₂ O	10	0
CH ₃ CN	10	0
CH ₃ CN	100	0
HFIP	10	0
CF ₃ CH ₂ OH	10	40
tBuOH	10	90
tBuOH	9	58
tBuOH	7	50
tBuOH	5	75



Optimisation

Scope

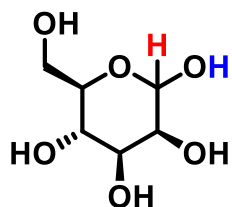
- Hexoses



D-Glucose

> 98 %

> 98 %



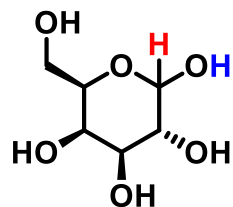
D-Mannose

> 98 %

> 98 %

Condition A: acetone, 5 mol% [Fe],
90 °C, 5 h

Condition B: 10 eq. acetone, *t*BuOH,
5 mol% [Fe], 90 °C, 5 h



D-Galactose

54 %

35 %

24 h

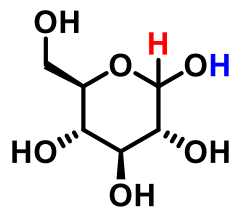
> 98 %

85 %

Optimisation

Scope

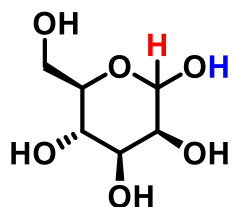
• Hexoses



D-Glucose

> 98 %

> 98 %



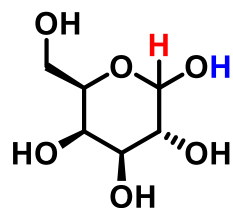
D-Mannose

> 98 %

> 98 %

Condition A: acetone, 5 mol% [Fe],
90 °C, 5 h

Condition B: 10 eq. acetone, *t*BuOH,
5 mol% [Fe], 90 °C, 5 h



D-Galactose

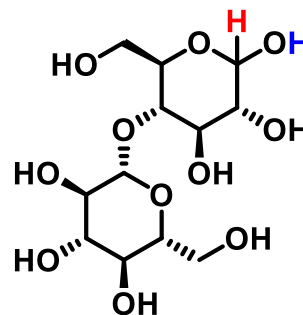
54 %

35 %

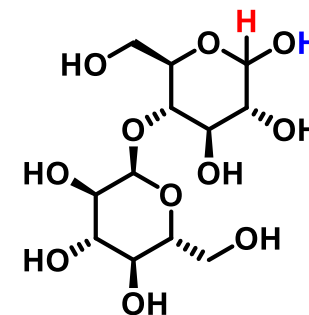
 24 h
> 98 %

85 %

Solubility issue?



D-cellobiose

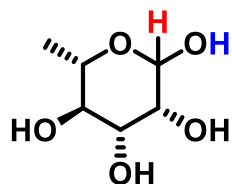


D-maltose

Optimisation

Scope

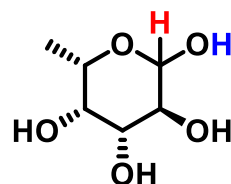
- Deoxy-sugars & pentoses



L-Rhamnose

> 98 %

94 %



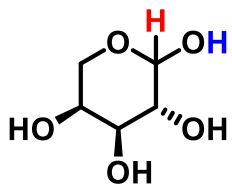
L-Fucose

> 98 %

90 %

Condition A: acetone, 2.5 mol% [Fe], 90 °C, 5 h

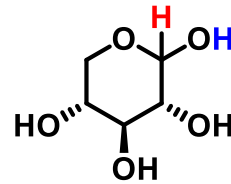
Condition B: 10 eq. acetone, *t*BuOH, 2.5 mol% [Fe], 90 °C, 5 h



L-Arabinose

> 98 %

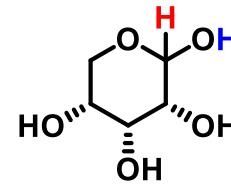
> 98 %



D-Xylose

> 98 %

> 98 %



D-Ribose

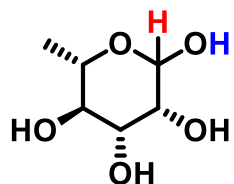
-

> 98 %

Optimisation

Scope

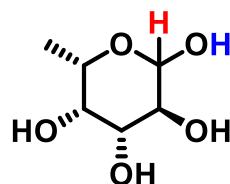
- Deoxy-sugars & pentoses



L-Rhamnose

> 98 %

94 %



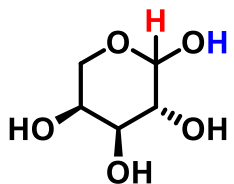
L-Fucose

> 98 %

90 %

Condition A: acetone, 2.5 mol% [Fe], 90 °C, 5 h

Condition B: 10 eq. acetone, *t*BuOH, 2.5 mol% [Fe], 90 °C, 5 h

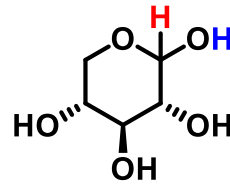


L-Arabinose

3 h

> 98 %

> 98 %

 -
90 %


D-Xylose

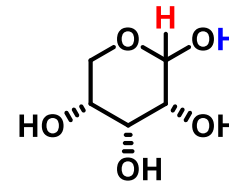
3 h

> 98 %

> 98 %

98 %

90 %



D-Ribose

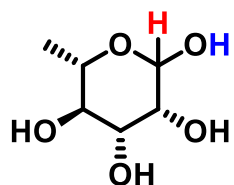
-

> 98 %

Optimisation

Scope

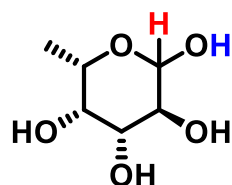
- Deoxy-sugars & pentoses



L-Rhamnose

> 98 %

94 %



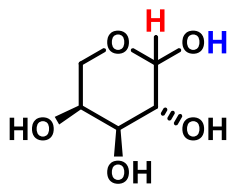
L-Fucose

> 98 %

90 %

Condition A: acetone, 2.5 mol% [Fe], 90 °C, 5 h

Condition B: 10 eq. acetone, *t*BuOH, 2.5 mol% [Fe], 90 °C, 5 h



L-Arabinose

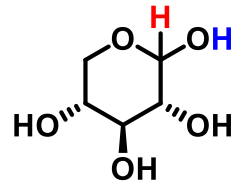
> 98 %

> 98 %

3 h

-

90 %



D-Xylose

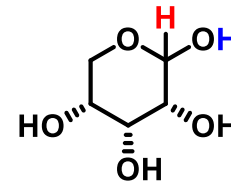
> 98 %

> 98 %

3 h

98 %

90 %



D-Ribose

-

> 98 %

500 mg

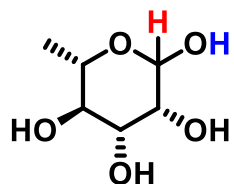
82 %

93 %

Optimisation

Scope

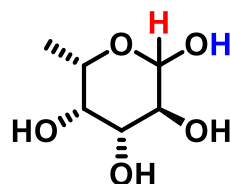
- Deoxy-sugars & pentoses



L-Rhamnose

> 98 %

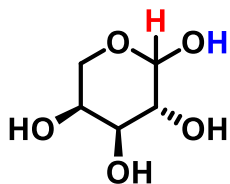
94 %



L-Fucose

> 98 %

90 %



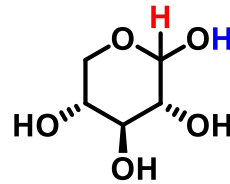
L-Arabinose

3 h

> 98 %

> 98 %

90 %



D-Xylose

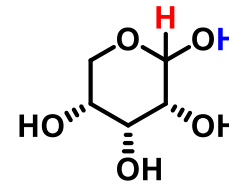
3 h

> 98 %

> 98 %

98 %

90 %



D-Ribose

-

> 98 %

500 mg

82 %

93 %

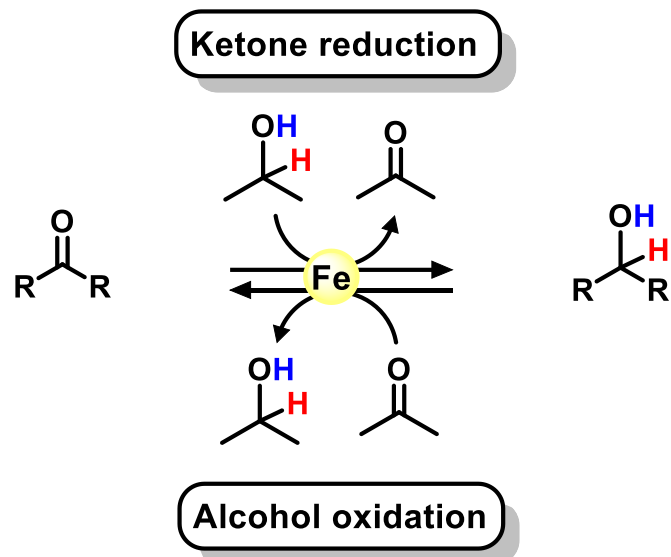
- ✓ Excellent selectivity & activity
- ✓ Hexoses & pentoses oxidation
- ✓ Mild conditions
- ✓ Greener solvent
- ✓ Earth abundant metal
- Excess of acceptor

Optimisation

Scope

Acceptor stoichiometry

- Transfer hydrogenation



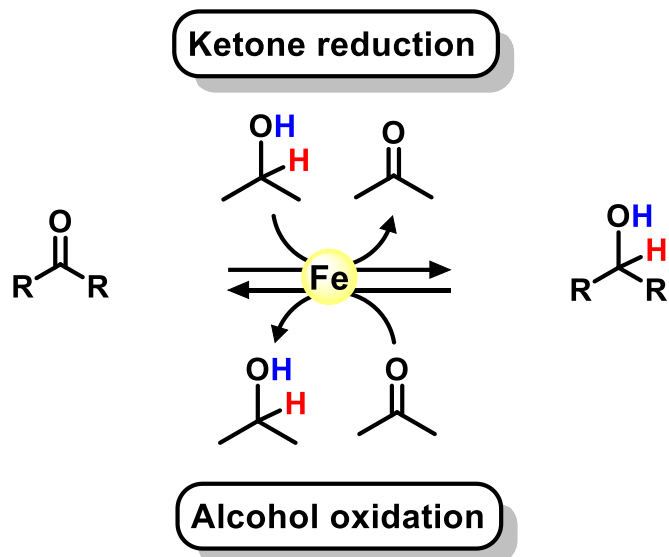
- Reversible process
- Excess of hydrogen donor / acceptor (often used as solvent)

Optimisation

Scope

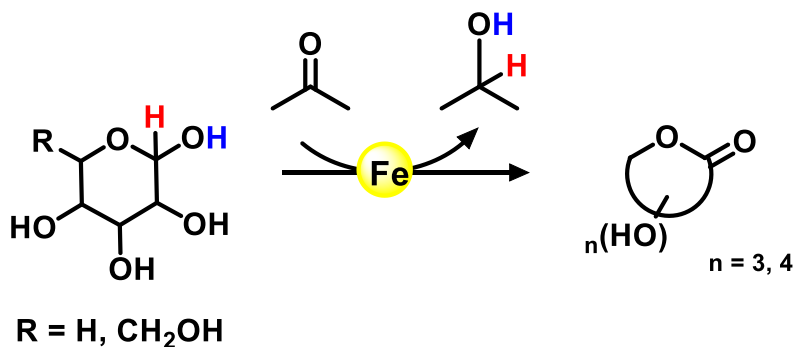
Acceptor stoichiometry

- Transfer hydrogenation



- Reversible process
- Excess of hydrogen donor / acceptor (often used as solvent)

- Oxidation of unprotected sugar via transfer hydrogenation



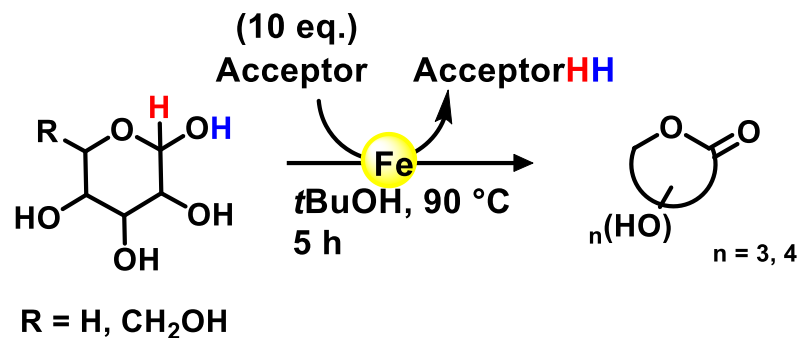
- Stable lactone – Irreversibility
- Stoichiometry of the acceptor?
- Increase the range of acceptors

Optimisation

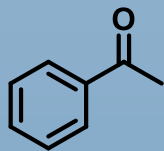
Scope

Acceptor stoichiometry

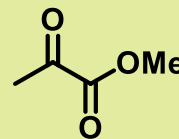
- Screening of acceptors



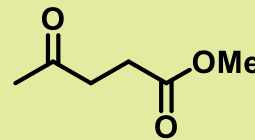
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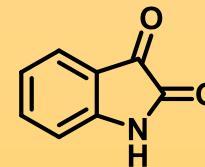
2



3



4



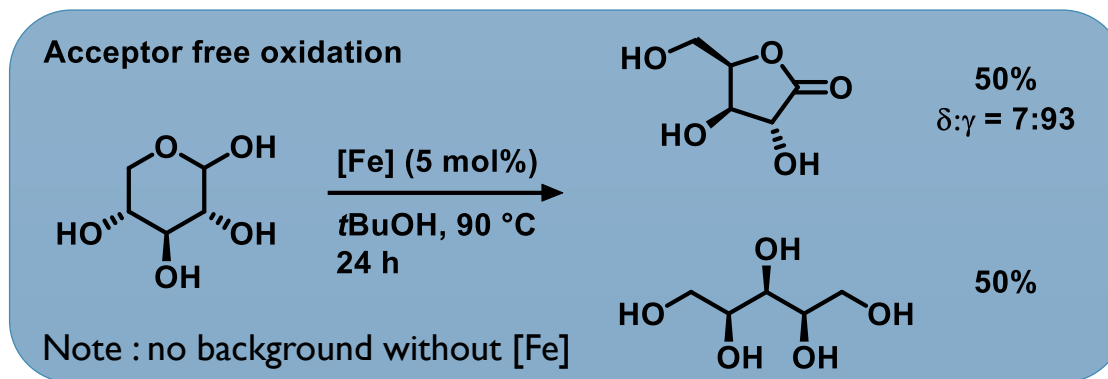
5

Optimisation

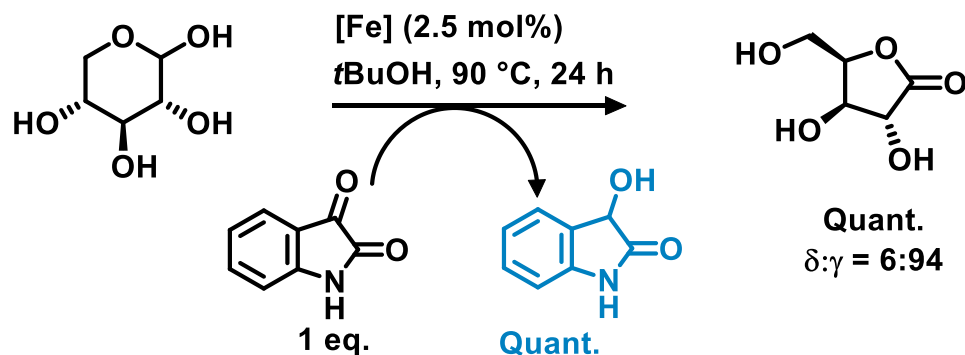
Scope

Acceptor stoichiometry

- Competitive disproportionation of xylose



- Stoichiometry - Isatin

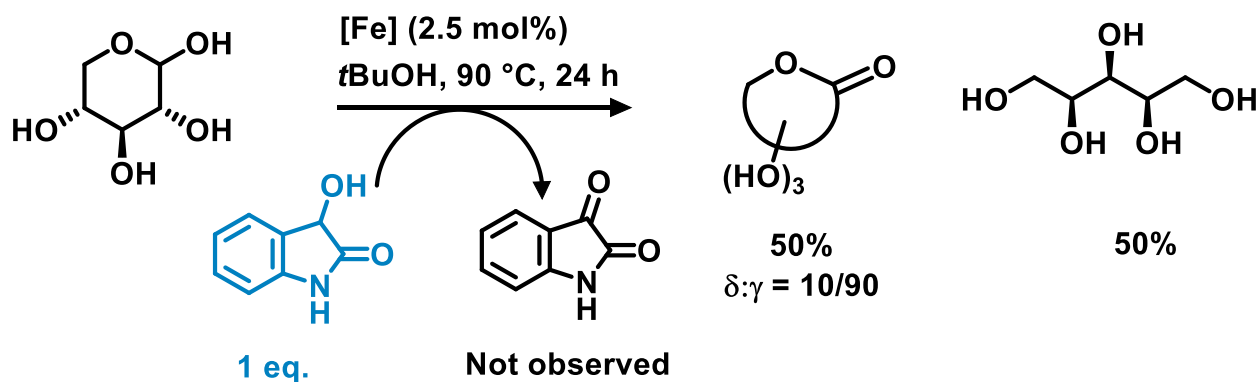


Optimisation

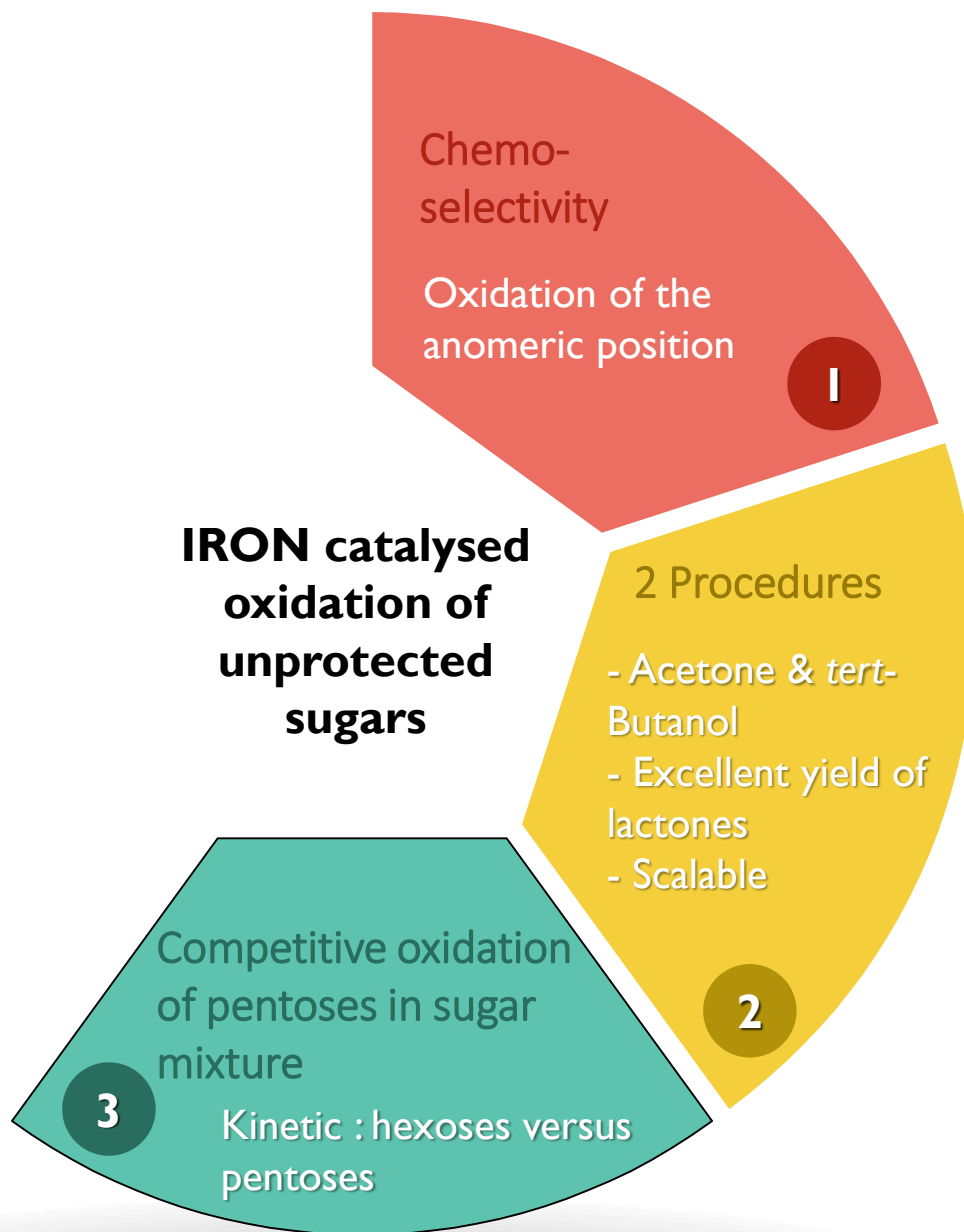
Scope

Acceptor stoichiometry

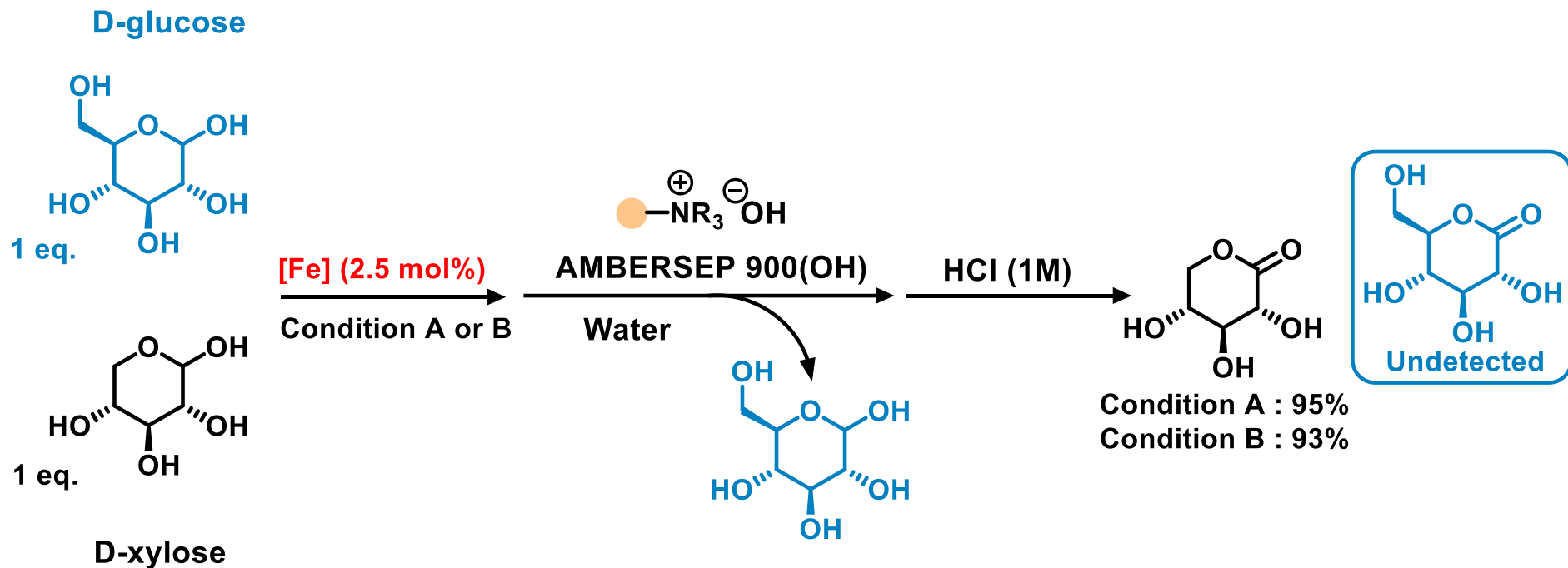
- 3-hydroxyoxindole as donor?



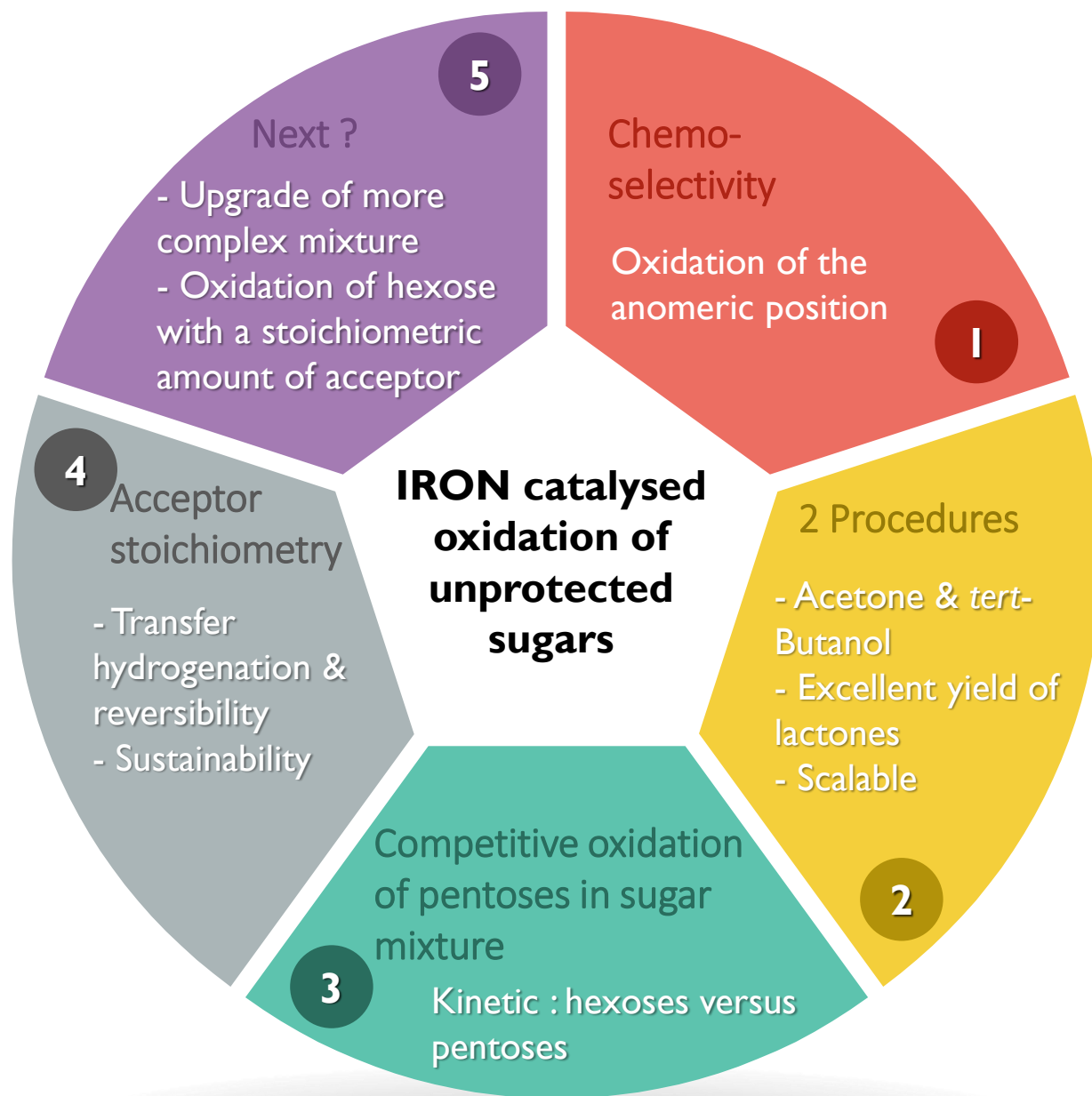
- Disproportionation favoured
- Irreversibility of the transfer hydrogenation process with isatin



- Sugars mixture

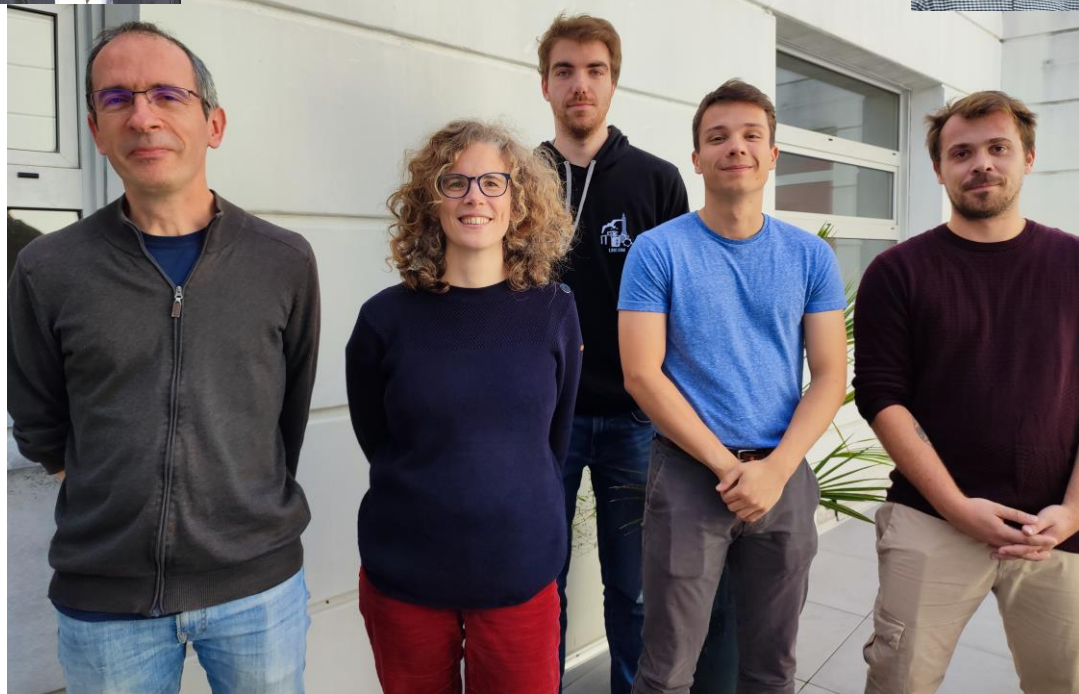


- Purification using an anion exchange resin
- Excellent yields of xylonolactones using procedure A and B





AKNOWLEDGEMENTS



- Collaborators

- David Branquet
- Fabian Cuffel
- Dr Mohamed Vall Sidi Boune
- Dr Uchchal Bandyopadhyay

- Dr Sébastien Comesse
- Dr Nicolas Hucher
- Dr Catherine Taillier
- Prof. Vincent Dalla
- Prof. Arnaud Martel (DFT calculations)

