





SONOCHEMISTRY & SONOCATALYSIS: Towards a Sustainable Approach to Oxidation & Hydrogenation Reactions at Mild Conditions





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CONVERSION OF BIO-BASED SUBSTRATES



Can we do Chemistry

- Assisted catalysis?
- At low temperature?
- Convenient reactions conditions
- Reusable and highly selective catalysts

✓ High selectivity

- ✓ Expensive
- ✓ Stringent process parameters
- ✓ Complicated downstream process

High selectivity, catalyst is reusable

Activity need to be improve

Mechanism is unknown

 $\checkmark\,$ Convenient reaction conditions and products separation

CONTRIBUTION OF NON-THERMAL TECHNOLOGIES

NON THERMAL TECHNOLOGIES



Hurdles

- Reaction mechanism
- Energy consumption
- Scale-up

Non-thermal technologies: non-thermal technologies do not involve an external source of heating and the chemical reaction can be activated either by the action of a pressure, electric or magnetic field, waves, light, to mention a few



Microwave



Ultrasound



Plasma

Can we convert biomass

- Without any solvent?
- Without any catalyst?
- At low temperature?





Milling

Photochemistry







Supercritical fluids



Research Vision for the Concept of Assisted-Catalysis Using Sonochemistry @ IC2MP





Strategies for improving existing catalytic reactions

for

CONTRIBUTION OF NON-THERMAL TECHNOLOGIES



ISLANDS OF CHEMISTRY



Chemistry: the interaction of energy and matter. The three axes represent **duration of the interaction**, **pressure**, and **energy per molecule**. The labeled islands represent the nature of the interaction of energy and matter in various different kinds of chemistry.

CAVITATION BUBBLE DYNAMICS



Symmetric Implosion of Cavitation Bubble

$$\tau = 0,915.R_{max} \cdot \sqrt{\frac{\rho}{P_m}} \cdot \left(1 + \frac{P_V}{P_m}\right)$$

 $P_m = P_A + P_h$

Pv= Vapour Pressure of the liquid





CAVITATION BUBBLE DYNAMICS



ChemSusChem, 2014, 7, 2774

CAVITATION BUBBLE AS A MICRO-REACTOR



CATALYTIC GLUCOSE OXIDATION: Conventional Approach





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SONOCHEMICAL OXIDATION OF BIO-BASED SUBSTRATES: GLUCOSE OXIDATION



Glucuronate salt



SONOCHEMICAL OXIDATION OF BIO-BASED SUBSTRATES: GLUCOSE OXIDATION



SONOCHEMICAL OXIDATION OF BIO-BASED SUBSTRATES: **SONOCATALYSIS - GLUCOSE OXIDATION**



Sonochemical Synthesis of CuO Nanoleaves

Sonochemical synthesis of CuO (HFUS):



- Triple transducer (total of 75 W)
- P₀ = 13.9 W
 P_{elect} = 70.4 W
 P_{acoust.vol} = 0.44W mL⁻¹



Hydrogen peroxide Quantification



H₂O₂ formation in the presence Fresh and Recycled catalyst







Ultrasound frequency 578 kHz, Amplitude 100 %, temperature 25 °C

SONOCHEMICAL OXIDATION GLUCOSE OVER CuO CATALYST

DFT calculations

- Without assistance of H[•], the ring-opening of glucose is less favorable energetically
 - \Rightarrow Can we suppress H• during the sonolysis of water?
 - \Rightarrow **Our approach**: combining CuO catalyst with HFUS to *in situ* trap H•
- DFT: Under HFUS conditions, the surface of CuO is covered by HO•
- \Rightarrow The surface lattice oxygen of CuO traps H[•], leaving a high coverage of HO[•] on the CuO surface
- ⇒ The HO• produced in water can replenish the lattice vacancies created on the surface of the catalyst







(80°C, 550 kHz, 10 wt % CuO, glucose oxidation 20 g L⁻¹, $P_{\text{acoust}} = 0.36$ W mL⁻¹)

- Selectivity to glucuronic = 82% (at 80% conv.) with CuO (LFUS)
- The heterogeneous nucleation of cavitation bubbles on a material surface is affected by the particle size *
 Lower particle size ⇒ enhanced cavitation bubble-solid particles contact angles
- Over CuO (HFUS) : switch of the selectivity! ⇒ selectivity to glucuronic = 95% (at 93% conv.).
 - \Rightarrow Enhanced interactions of the radicals and the surface of the catalyst

* Chem. Mater., **2014**, 26, 2244

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NMR & MS ANALYSIS OF CRUDE REACTION PRODUCT



Recycling of the CuO (HFUS) 3.5-4.7 µm



(80°C, 550 kHz, 10 wt % CuO_{HFUS}, glucose oxidation 20 g L⁻¹, $P_{\text{acoust}} = 0.36$ W mL⁻¹)

 \Rightarrow CuO (HFUS) stable \Rightarrow Abrasion drastically limited under HFUS (confirmed by SEM)

Challenge: Direct synthesis of hydrazine from ammonia

$$NH_3 \xrightarrow{?} N_2H_4$$
$$\Delta G=16,5 \text{ kJ.mol}^{-1}$$

Major hurdles:

High N-H bond dissociation energy of ammonia (435 kJ.mol⁻¹)

Low thermal stability of hydrazine (ΔG =-150 kJ.mol⁻¹)

Catalyst able to activate NH₃ will inevitably decompose hydrazine



Is it possible to replace a chemical activation by a physical activation of NH₃?



ACTIVATION OF NH3 TOWARDS HYDRAZINE FORMATION





Dr. Anaelle Humblot





100 ml of 5 wt% ammonia solution or 100 ml of water + NH₃ bubbling 30°C High frequency ultrasound 525 kHz





Hydrazine production from ammonia



N₂H₄ formation rate > decomposition rate

ACTIVATION OF NH3 TOWARDS HYDRAZINE FORMATION



Effect of Gas flow



Influence of gases on the initial formation rate of N₂H₄ (10 ml/min NH₃ + 20 ml/min gas, 525 kHz, 0.17 W/mL, 30°C). All reactions were conducted at atmospheric pressure





Effect of reaction bulk temperature



Concentration of hydrazine as a function of the reaction time (bubbling of NH₃ at 30 ml/min, 525 kHz, 0.21 W/mL) at 30° C and 60° C. 0.17 W/mL at 60° C













Hydrogenation of 1-Octene in an Aqueous solution of NH₃ (5 wt%)





kinetic profile and blank experiments (30°C, 525 kHz, NH₃ 5 wt%, under air)

A. Humbot, P.N. Amaniampong, T. Chave, S. Streiff, F.Jerome. Angew. Chem. Int. Ed. 2022

Hydrogenation of 1-Octene in an Aqueous solution of NH₃ (5 wt%)







Proposed reaction mechanism illustrating the implosion of aqueous NH₃ filled cavitation bubbles on the surface of activated carbon coated with 1-octene and associated reactions





3,50E-04 3,00E-04 N_2H_4 formation rate (mol.L⁻¹.h⁻¹) 2,50E-04 2,00E-04 1,50E-04 1,00E-04 5,00E-05 0,00E+00 0,05 0,10 0,15 0,20 0,25 0,00 Acoustic power (W/mL)

Direction for future studies

The formation rate of hydrazine increases exponentially when increasing the acoustic power

Development of a continuous ultrasonic reactor to increase the acoustic power and the production of hydrazine



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Merci pour votre attention



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